

Name: _____

Fluid I.D. : _____

Solutions:

1)

$$\tau_w = \rho u^*{}^2 \Rightarrow 122 = 998u^*{}^2 \Rightarrow u^* = 0.35 \text{ m/s}$$

$$a) V_c = u^* \left(\frac{1}{\kappa} \ln \left(\frac{Ru^*}{\nu} \right) + B \right) = 0.35 \left(\frac{1}{0.41} \ln \left(\frac{998 * 0.045 * 0.35}{0.001} \right) + 5 \right) = 10 \text{ m/s}$$

$$b) V = u^* \left(2.44 \ln \left(\frac{Ru^*}{\nu} \right) + 1.34 \right) = 8.72 \text{ m/s}$$

$$Q = AV = 0.055$$

$$c) \Delta P = 2\tau_w \Delta L / R = 542000 \text{ Pa}$$

2)

Solution: For water at 20°C, take $\rho = 998 \text{ kg/m}^3$ and $\mu = 0.001 \text{ kg/m}\cdot\text{s}$. For cast iron, $\epsilon \approx 0.26 \text{ mm}$, hence $\epsilon/d = 0.26/50 \approx 0.0052$. The minor loss coefficients are Entrance: $K \approx 0.5$; 5-cm($\approx 2''$) open globe valve: $K \approx 6.9$

The flow rate is known, hence we can compute V, Re, and f:

$$V = \frac{Q}{A} = \frac{0.004}{(\pi/4)(0.05)^2} = 2.04 \frac{\text{m}}{\text{s}}, \quad \text{Re} = \frac{998(2.04)(0.05)}{0.001} \approx 102000, \quad f \approx 0.0316$$

The turbine head equals the elevation difference minus losses and exit velocity head:

$$h_t = \Delta z - h_f - \sum h_m - \frac{V^2}{2g} = 40 - \frac{(2.04)^2}{2(9.81)} \left[(0.0316) \left(\frac{125}{0.05} \right) + 0.5 + 6.9 + 1 \right] \approx 21.5 \text{ m}$$

$$\text{Power} = \rho g Q h_t = (998)(9.81)(0.004)(21.5) \approx \mathbf{840 \text{ W}} \quad \text{Ans.}$$

3) $\sum F_z = 0 \Rightarrow T + D + F_B = W$

Where:

T=tension force

F_B = Bouyancy Force

D=friction Drag

W= weight

$$F_B = \rho_w g * V = 9810 * 0.003 * 1 * 3 = 88.3 \text{ N}$$

$$D = C_D (0.5 \rho A V^2)$$

$$\text{Re} = \rho V L / \mu = 4.6e6 \text{ Turbulent flow}$$

$$C_D = 0.031 / \text{Re}^{1/7} = 3.46e-3$$

$$D = 0.003 * 2 * 3 * 1000 * 36 / 2 = 324 \text{ N}$$

$$T = 500 - 324 - 88.3 = 87.4 \text{ N}$$

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4)

$$\Sigma M_o = F_a(0.1 \sin 45^\circ) - W_a(0.1 \cos 45^\circ) - F_b(0.1 \sin 45^\circ) + W_b(0.1 \cos 45^\circ) = 0$$

For 45° , there are nice cancellations to obtain $\therefore F_a - F_b = W_a - W_b$, or:

$$C_{Da} \frac{\rho}{2} U^2 \frac{\pi}{4} D_a^2 - C_{Db} \frac{\rho}{2} U^2 \frac{\pi}{4} D_b^2 = (SG)\rho_{\text{water}}g \frac{\pi}{6} D_a^3 - (SG)\rho_{\text{water}}g \frac{\pi}{6} D_b^3$$

Assuming that $C_{Da} = C_{Db} \approx 0.47$ ($Re < 250000$), we may easily solve for air velocity:

$$U^2(0.47) \left(\frac{1.225}{2} \right) \frac{\pi}{4} [(0.02)^2 - (0.01)^2] = (7.86)(9790) \frac{\pi}{6} [(0.02)^3 - (0.01)^3]$$

$$\text{Solve for } U = \sqrt{4158} \approx \mathbf{64 \text{ m/s}} \quad \text{Ans.}$$

We may check that $Re_{\text{max}} = 1.225(64)(0.02)/1.78E-5 \approx 89000$, OK, $C_D \approx 0.47$.

5)

$$\psi = U_\infty \sin \theta (r - a^2/r) = U_\infty y - U_\infty y \frac{a^2}{x^2 + y^2} = U_\infty y \left(1 - \frac{a^2}{x^2 + y^2} \right)$$

At $x = \infty$: $y = h$

At $x = 0$: $y = h + a/3$

Those points are on the same streamline:

$$\text{a) } \psi = U_\infty h = U_\infty (h + a/3) \left(1 - \frac{a^2}{(h + a/3)^2} \right) \Rightarrow h = \frac{8}{3} a$$

$$\text{b) } U_{\text{max}} = U_\infty \sin 90 \left(1 + \frac{a^2}{(h + a/3)^2} \right) = U_\infty \left(1 + \frac{a^2}{(3a)^2} \right) = \frac{10}{9} U_\infty$$